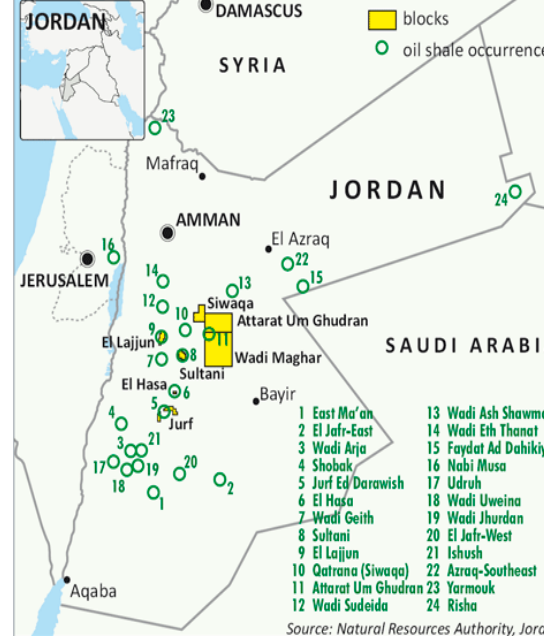
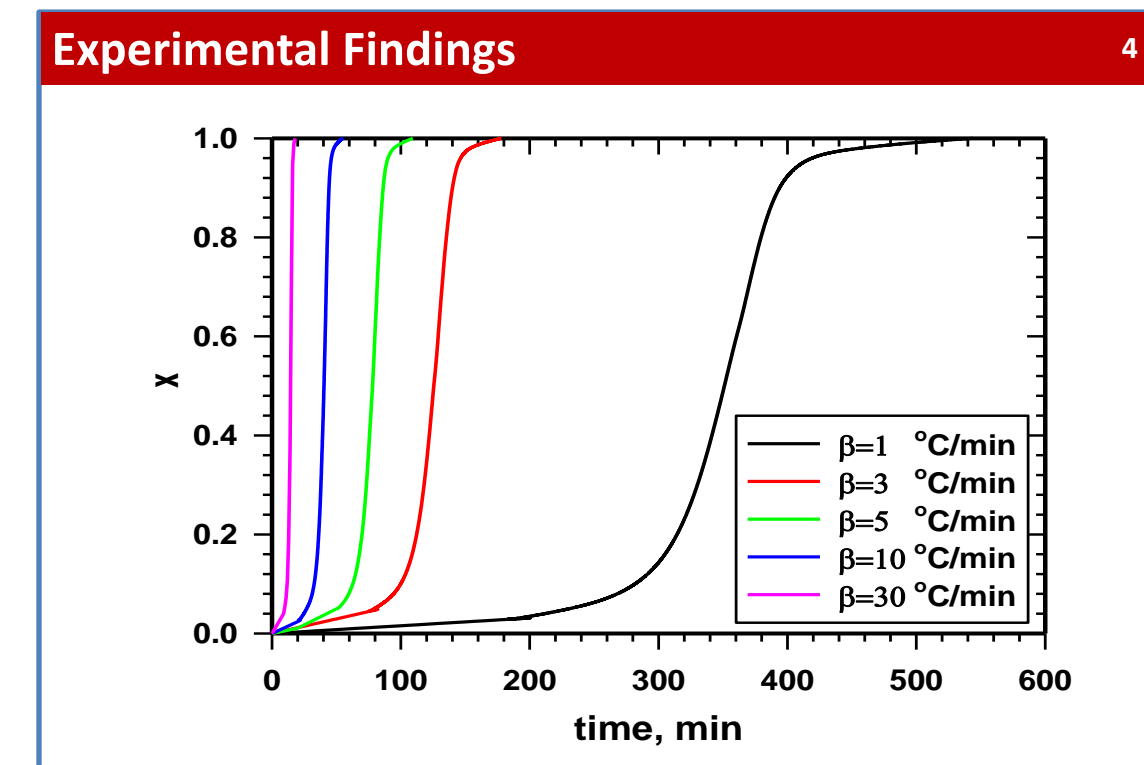

A New Approach for Kinetic Modelling of El Lajjun Oil Shale Extracted Kerogen
 Mohammad Al-Shannag
 Department of Chemical Engineering
 Faculty of Engineering Technology,
 Al-Balqa Applied University
 Amman, Jordan
 October, 2012

Oil Shale in Jordan

- Jordan is very rich in oil shale deposits.
- The main sites are located at El Lajjun, Sultani, and Jurf-Ed-Darawish located in west central Jordan; 20 to 75 km east of the Dead Sea.
- Jordan reserves of oil shale is around 50 billion tons.

Traditional Kinetic Approach

Previous studies analyzed the non-isothermal kinetics of oil shale and its kerogen using the Arrhenius equation:

$$\frac{dx}{dt} = \beta \frac{dX}{dT} = Ae^{-E/RT} f(x)$$

where dx/dt is the rate of conversion for Thermogravimetric experiment at constant heating rate (β), E is the apparent activation energy, A is the pre-exponential factor and R is the gas constant.

New Kinetic approach

The present work analyzed the non-isothermal kinetics of El Lajjun oil shale kerogen using Gaussian function of the form:

$$\frac{dx}{dt} = \beta \frac{dX}{dT} = ae^{-0.5\left(\frac{x-c}{b}\right)^2}$$

where a , b , and c are the kinetic model parameters.

Findings of New Kinetic Model

The resulting kinetic parameters at different heating rates:

β ; °C/min	a	b	c
1	0.0124	0.2165	0.533
3	0.0356	0.2207	0.5472
5	0.0593	0.2267	0.5422
10	0.1237	0.2182	0.5569
30	0.3750	0.2035	0.5298

Experimental Method

- Oil shale used in this study was obtained from El-Lajjun area in Jordan.
- Kerogen was isolated from raw oil shale by sequential HCl and HCl/HF digestion.
- Kerogen samples were pyrolyzed in a Thermogravimetric analyzer at different heating rates: $\beta=1, 3, 5, 10,$ and 30 °C/min up to a temperature of around 550 °C.

Kerogen Conversion Fraction ; X

$$X = \frac{W_0 - W_t}{W_0 - W_f}$$

X : Conversion fraction
 W_0 : Initial mass of the sample
 W_t : Mass of the sample at t time
 W_f : Final mass of the sample

Traditional Kinetic Approach

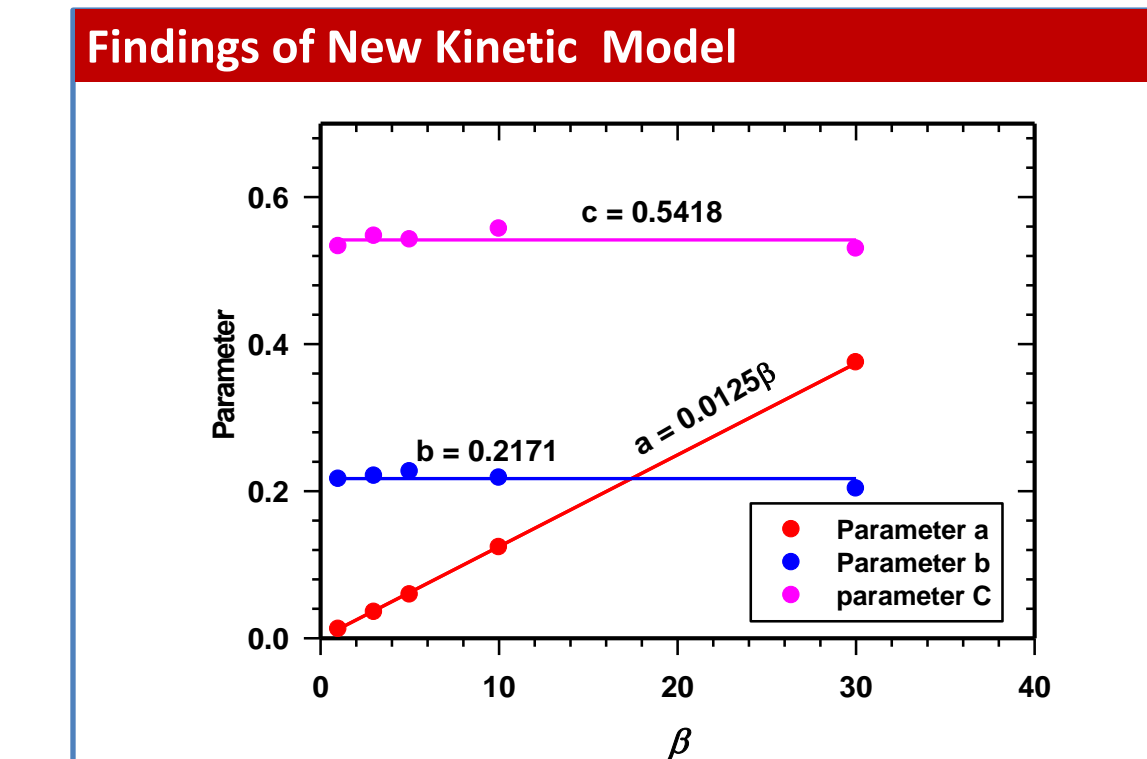
The apparent activation energy and the pre-exponential factor are estimated using various mathematical strategies such as:

- Friedman method.
- Kissinger-Akahira-Sunose (KAS) method.
- Flynn-Wall-Ozawa (FWO) method.
- Coats and Redfern method.
- etc...

New Kinetic approach

To find the proposed model parameters:

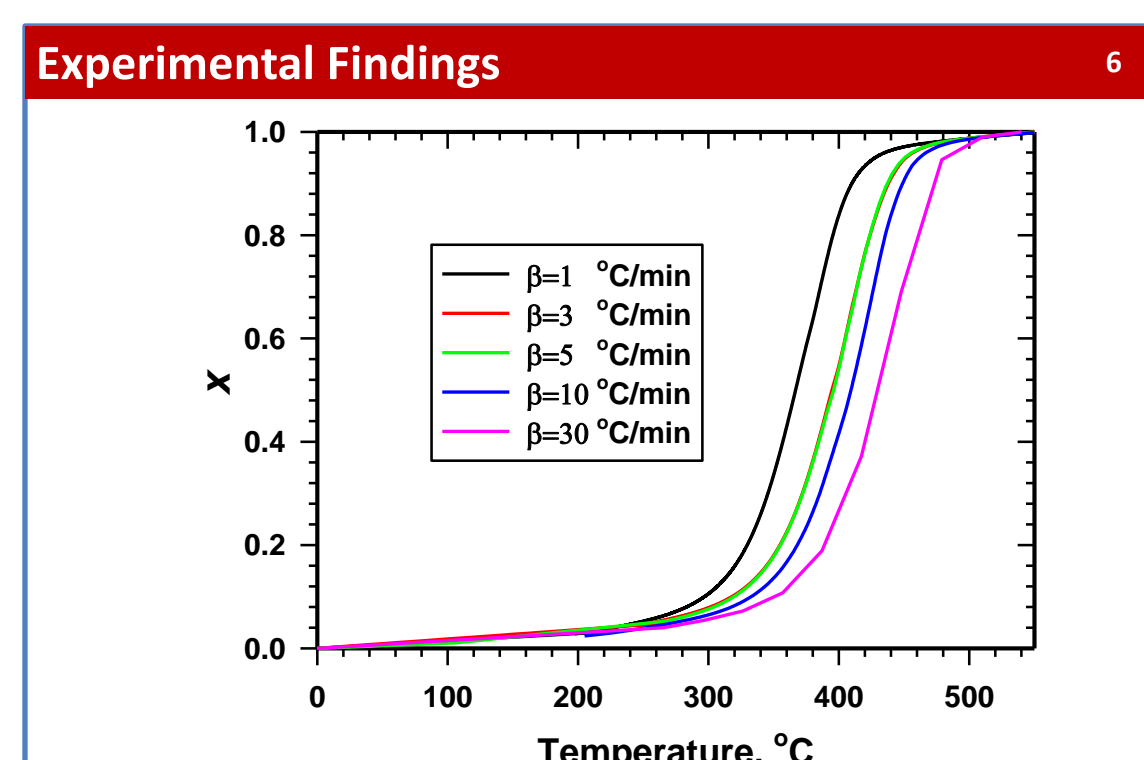
- The value of dx/dt has been calculated at each time point using fourth-order finite difference schemes.
- The resulting dx/dt values has been plotted against the corresponding x values.
- Least-square method has been used to estimate the three model parameters.



Experimental Findings

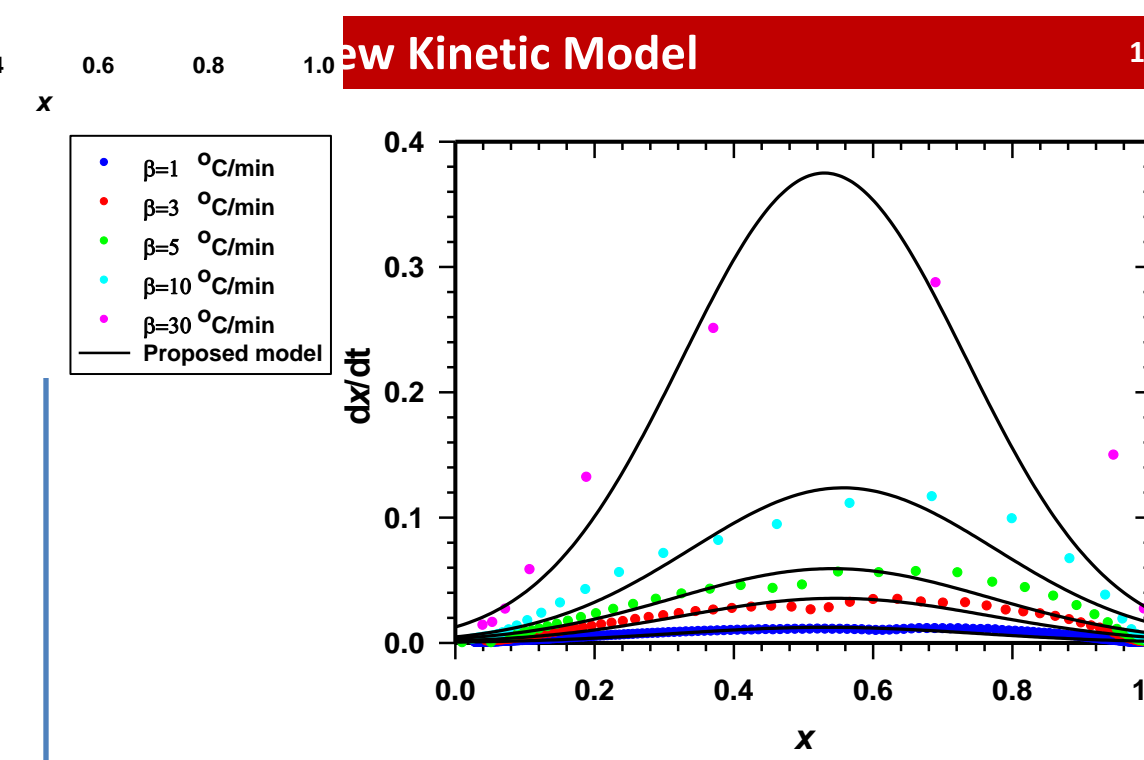
Mass composition of oil shale samples:

Moisture content	1.85%
Soluble organics before acid treatment	3.17%
Carbonate	46.46%
Silica and clay minerals	26.94%
Soluble organics after acid treatment	1.09%
Kerogen and insoluble minerals	20.49%



Kinetic approach

- Pyrolysis of oil shale kerogen involves multiple reactions (no unique activation energy).
- Inaccurate kinetic findings of many previous works due to the unsafe assumption: fixing one E parameter in the mathematical formulations.
- The present study proposed a new approach to avoid such mathematical conflict.



Conclusions

- Non-isothermal pyrolysis of El Lajjun oil shale kerogen can be modelled correctly as:

$$\frac{dx}{dt} = \beta \frac{dX}{dT} = 0.0125\beta e^{-0.5\left(\frac{x-0.5418}{0.2171}\right)^2}; (\beta \leq 30; T \leq 550 \text{ °C})$$

- The present study shows that the pre-exponential parameter of the proposed Gaussian model increases linearly with increasing heating rate. The other two-exponential parameters are constant.
- It is recommended to try Gaussian law to model oil shale pyrolysis.