

***Options for sulfur dioxide removal using oil shale waste and natural materials: An experimental study***

Mohammad Al-Harashsheh<sup>1</sup>, Marwan Batiha<sup>1</sup>, Khalid Al-Tarawneh<sup>1</sup>, Adnan Al-Harashsheh<sup>2</sup>, Reyad Al-Shawabkiah<sup>3</sup>, Muhannad Hararah<sup>1</sup>

<sup>1</sup>*Faculty of Engineering, Al-Hussein Bin Talal University, Jordan,* <sup>2</sup>*Faculty of Engineering, Mutah University, Jordan,* <sup>3</sup>*King Fahd University for Petroleum and Materials, Chemical Engineering Department, Saudi Arabia*

Oil shale combustion is a promising option for Jordanian oil shale utilization. Restrictions on the exploitation and utilization of this resource are partly due to the high sulfur content of the oil shale, which leads to production of large quantities of sulfur dioxide during combustion. Mitigation of sulfur dioxide prior to effluent gas release is important for maintaining air quality and preventing environmental problems like acid rain. A number of effluent gas desulfurization techniques are available. These can be broadly classified into four categories: absorption of SO<sub>2</sub> in liquids, absorption by moist particles, gas phase conversion of SO<sub>2</sub>, and sorption by solids. Solid-phase sorption has been examined in this study for SO<sub>2</sub> removal during oil shale combustion using oil shale ash and Jordanian zeolitic tuff. Jordanian oil shale contains large quantities of carbonate minerals and when combusted a highly alkaline ash is produced that can be used as a sorbent for SO<sub>2</sub> abatement. Jordan also has considerable reserves of zeolitic tuff containing a variety of zeolite minerals including phillipsite, chabazite and faujasite. Oil shale ash combusted over a range of temperatures (550-950°C) and zeolitic tuff samples were sieved into different particle size fractions and the fractions of both materials were characterized by X-ray Diffraction (XRD), X-Ray Fluorescence (XRF) and Scanning Electron Microscopy (SEM). The surface area was also measured. Samples were placed in quartz tubes and heated to a specified temperature and then held for 15 minutes. SO<sub>2</sub> gas was passed through the tube and the concentration of non-adsorbed sulfur dioxide was measured at the outlet. The adsorption capacity of zeolitic tuff was found to increase with increasing temperature up to 200-250°C and then decreased at higher temperatures. It was also found that drying zeolitic tuff had a considerable effect on SO<sub>2</sub> adsorption capacity and breakthrough time. The adsorption capacity of zeolitic tuff increased with the decreasing particle size due to the increase of active surface area. For SO<sub>2</sub> sorption to oil shale ash, it was found that maximum SO<sub>2</sub> uptake occurred in the presence of O<sub>2</sub>. The formation of CaSO<sub>4</sub> was confirmed in oil shale ash sorption experiments. Finally, the uptake capacity of oil shale ash was found to be highest at 700°C.